

IMPACT OF ALTERNATIVE DISPERSION MODEL VALIDATION METHODS:

**A Case Study on the LNG Model Validation
Database using DRIFT**

Simon Gant, Simon Coldrick, Graham Tickle and
Harvey Tucker

Harmo-17 Conference, 9-12 May 2016

Budapest, Hungary

Contents

- Background
 - Regulation of LNG facilities
 - LNG Model Evaluation Protocol
 - Maximum arc-wise concentrations
- Aims
- Methodology
- Results
- Conclusions

Regulation of LNG Facilities

- US Federal Regulation 49 CFR 193 on Liquefied Natural Gas (LNG) facilities
- NFPA 59A (2001) “Standard for the Production, Storage, and Handling of LNG”
- Applicants required to calculate size of exclusion zones, based on vapour cloud dispersion distance to $\frac{1}{2}$ Lower Flammability Limit (LFL) for design spills
- Approved dispersion models (until 2011): DEGADIS, FEM3A
- Alternative dispersion models approved by US Pipelines and Hazardous Materials Safety Administration (PHMSA) using the NFPA LNG Model Evaluation Protocol



© US DOT PHMSA

LNG Model Evaluation Protocol

- 2007 ← LNG Model Evaluation Protocol (Ivings *et al.*, 2007)
- 2008 ← LNG Model Validation Database (Coldrick *et al.*, 2008)
- 2009 ← Review of LNG Source Models (Webber *et al.*, 2009)
- 2010 ← { LNG Model Validation Database, Version 11 (Coldrick *et al.*, 2010)
PHMSA Advisory Bulletin PHMSA-2010-0226
- 2011 { DEGADIS 2.1 Evaluation (FERC, 2011)
- 2012 { PHAST v6.6/6.7 Evaluation (PHMSA, 2011)
- 2013 { FLACS v9.1r2 Evaluation (PHMSA, 2011)
- 2014
- 2015
- 2016 ← LNG Model Validation Database, Version 12 (Stewart *et al.*, 2016)

LNG Model Validation Database



Trial Name	Sheet number in the Database	Trial number	Field (F) or Wind tunnel (WT)	Obstructed (O) or unobstructed (U)	Atmospheric stability	Substance released	Dispersion over water (W) or land (L)
Maplin Sands, 1980	1	27	F	U	C-D	LNG	W
	2	34			D		
	3	35			D		
Burro, 1980	4	3	F	U	B	LNG	L
	5	7			D		
	6	8			E		
	7	9			D		
Coyote, 1981	8	3	F	U	B-C	LNG	L
	9	5			C-D		
	10	6			D		
Falcon, 1987	11	1	F	O	G	LNG	L
	12	3			D		
	13	4			D-E		
Thorney Island 1982-4	14	45	F	U	E-F	Freon 12 & Nitrogen	L
	15	47			F		
CHRC, 2006	16	A	WT	U	D	Carbon Dioxide	L
	17	B		O	D		
	18	C		O	D		
BA-Hamburg	19	Unobstructed (DA0120)	WT	U	D	Sulfur Hexafluoride	L
	20	Unobstructed (DAT223)		U	D		
	21	Upwind fence (039051)		O	D		
	22	Upwind fence (039072)		O	D		
	23	Downwind fence (DA0501)		O	D		
	24	Downwind fence (DA0532)		O	D		
	25	Circular fence (039094/039095)		O	D		
	26	Circular fence (039097)		O	D		
	27	Slope (DAT647)		U	D		
	28	Slope (DAT631)		U	D		
29	Slope (DAT632)		U	D			
30	Slope (DAT637)		U	D			
BA-TNO	31	TUV01	WT	U	D	Sulfur Hexafluoride	L
	32	TUV02		O	D		
	33	FLS		U	D		

A	B	C
1 Trial Name		
2 Burro 3		
3 Test identifier		
4 BU3		
5 Date of test		
6 July 2 1980		
7 Origin of data		
8 MDA/Rediphen/Ermak et al 1988		
9 Date of inclusion, last revision		
10 August 12 2008, August 07 2009		
11 Description of test		
Continuous release of 34 m ³ LNG into 58m diameter water basin		
12		
13 TRIAL DATA		
14		
15 Substance released		Units
16 Substance	LNG	
17 Composition	92.5% methane, 6.2%	mol%
18 Molecular weight	17.26	kg/kmol
19 Density	432.7	kg/m ³
20 Normal boiling point	111.6	K
21 Latent heat of evaporation	511900	J/kg
22 Specific heat for vapor	2238	J/kg-K
23 Specific heat for liquid	3348.5	J/kg-K
24		
25 Release conditions		Units
26 Exit pressure	not applicable	
27 Spill temperature	111.6	K
28 Source diameter	not measured	
29 Source elevation	-1.5	m
30 Source type	evaporating pool	
31 Storage phase	liquid	
32 Spill containment diameter	58	m
33 Spill rate	87.98	kg/s
34 Spill duration	167	s
35 Total quantity released	14712	kg
36 Initial concentration	100	%
37 Exit pipe height above water surface	1.5	m
38		
39		
40		
41 Atmospheric conditions		Units
42 Ambient temperature	307.75	K
43 Measuring height of ambient temperature	1	m
44		
45		
46		
47		
48		
49		
50		
51		
52		
53		
54		
55		
56 MODEL OUTPUT		
57		
58 Arc-wise data		
59		
60		
61		
62		
63		
64		
65		
66		
67		
68		
69		
70		
71		
72		
73		
74		
75		
76		
77		
78		
79		
80		
81		
82		
83		
84		
85		
86		
87		
88		
89		
90		
91		
92		
93		
94		
95		
96		
97		
98		
99		
100		
101		
102		
103		
104		
105		
106		
107		
108		
109		
110		
111		
112		
113		
114		
115		
116		
117		
118		
119		
120		
121		
122		
123		
124		
125		
126		
127		
128		
129		
130		
131		
132		
133		
134		
135		
136		
137		
138		
139		
140		
141		
142		
143		
144		
145		
146		
147		
148		
149		
150		
151		
152		
153		
154		
155		
156		
157		
158		
159		
160		
161		
162		
163		
164		
165		
166		
167		
168		
169		
170		
171		
172		
173		
174		
175		
176		
177		
178		
179		
180		
181		
182		
183		
184		
185		
186		
187		
188		
189		
190		
191		
192		
193		
194		
195		
196		
197		
198		
199		
200		

Previous Evaluations

FLACS v9.1

PHAST v6.6/6.7

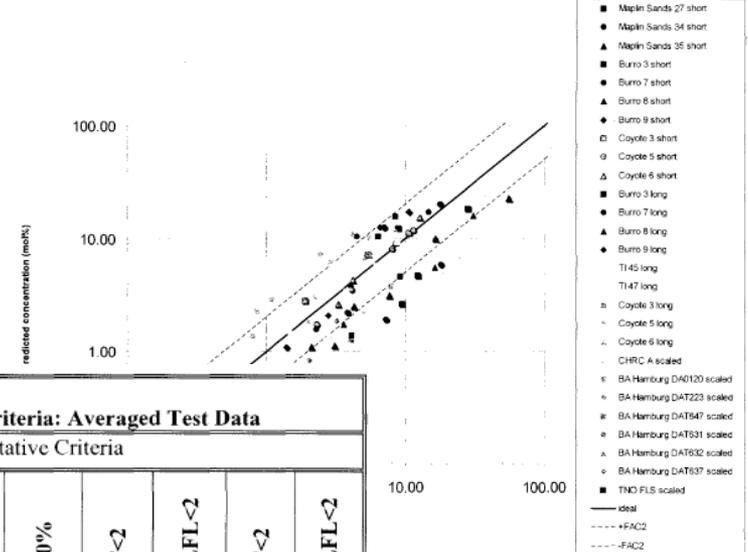
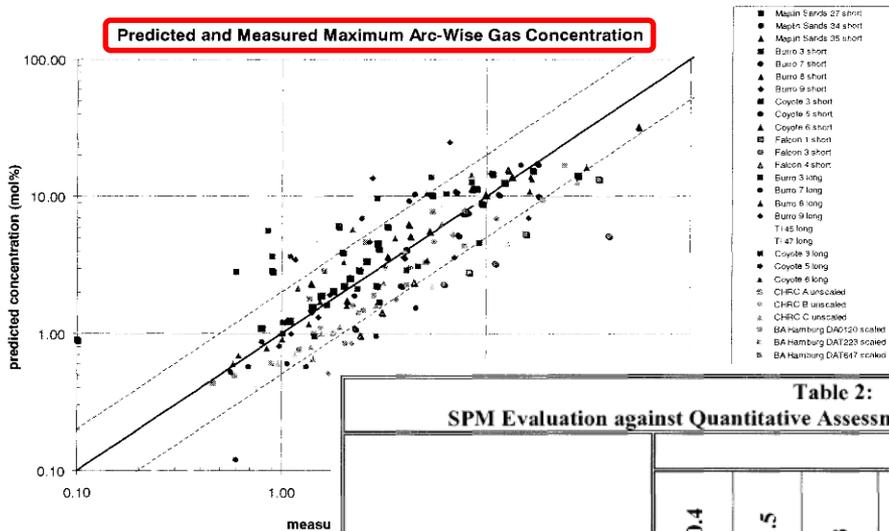


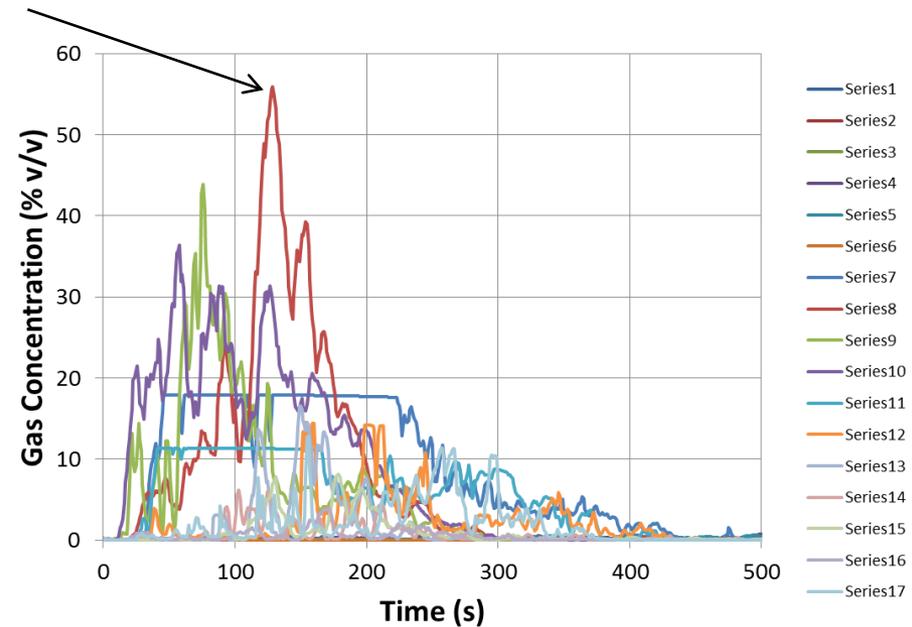
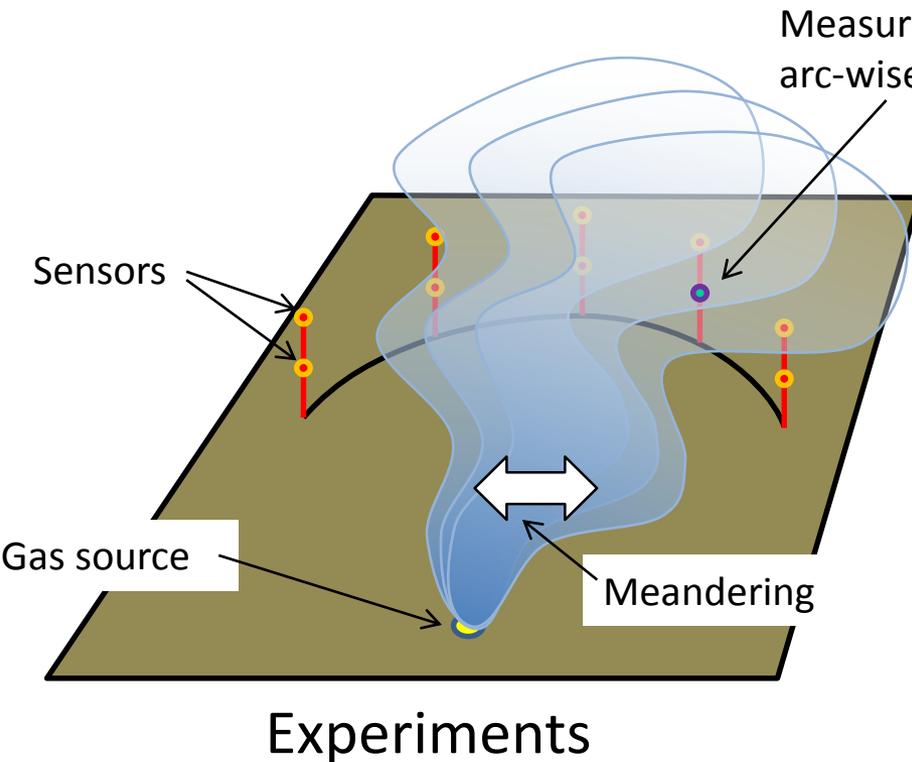
Figure 1 Predicted Cor

Table 2:
SPM Evaluation against Quantitative Assessment Criteria: Averaged Test Data

Data Set	Quantitative Criteria								
	-0.4<MRB<0.4	0.67<MG<1.5	MRSE<2.3	VG<3.3	FAC2 >50%	0.5<CSF<2	0.5<CSF_LFL<2	0.5<DSF<2	0.5<DSF_LFL<2
Maximum Arc-Wise Gas Concentration									
Maplin Sands 27 (short)	1.24	2.54	1.20	5.16	0%	0.64	0.38	N/A	N/A
Maplin Sands 34 (short)	1.10	3.45	1.21	4.70	0%	0.29	0.24	N/A	N/A
Maplin Sands 35 (short)	0.89	2.61	0.79	2.51	0%	0.38	0.38	N/A	N/A
Burro 3 (short)	0.06	1.06	0.14	1.15	100%	1.01	2.17	N/A	N/A

Measured Concentration

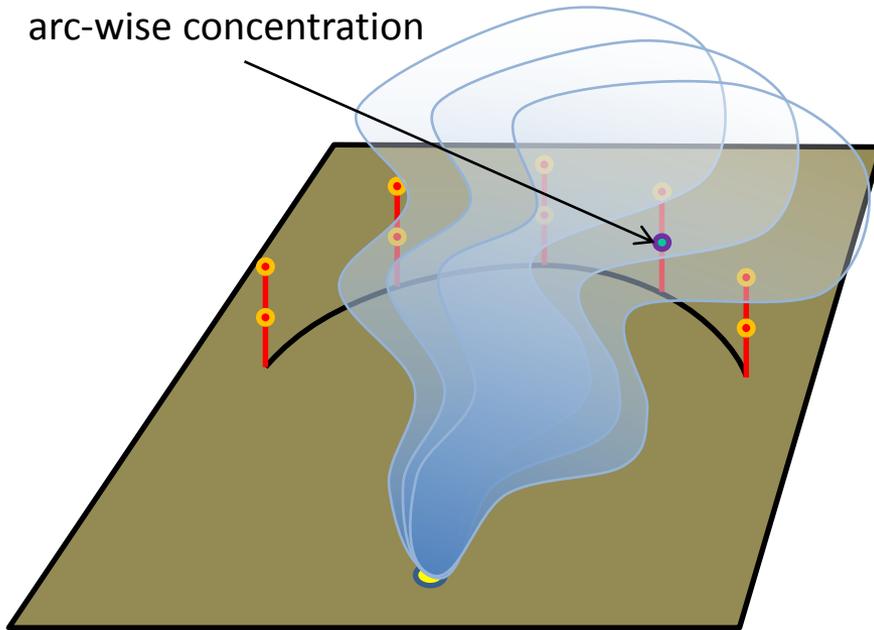
Maximum Arc-Wise Concentration



Example: Burro 8 sensors on arc at distance of 57 m

Maximum Arc-Wise Concentration

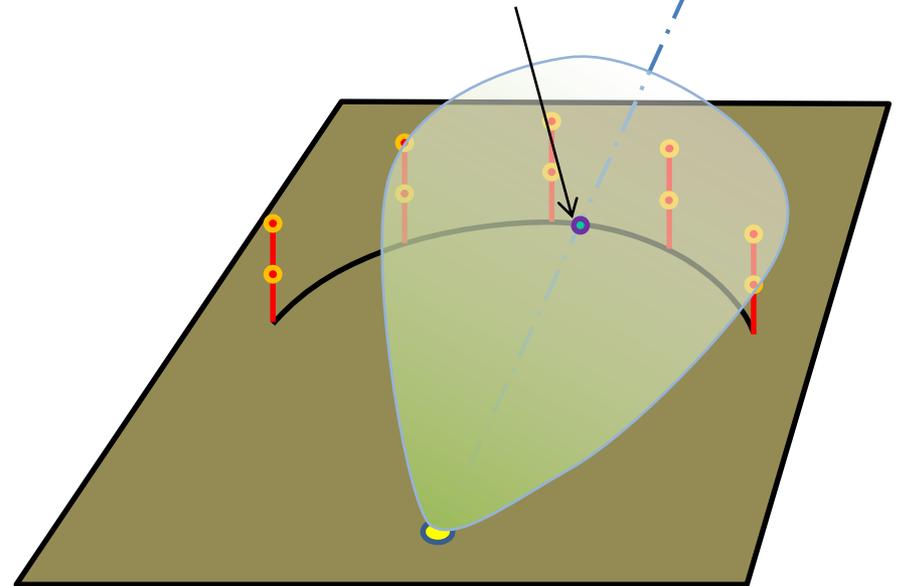
Measured maximum arc-wise concentration



Experiments

Predicted maximum arc-wise concentration

Cloud centreline

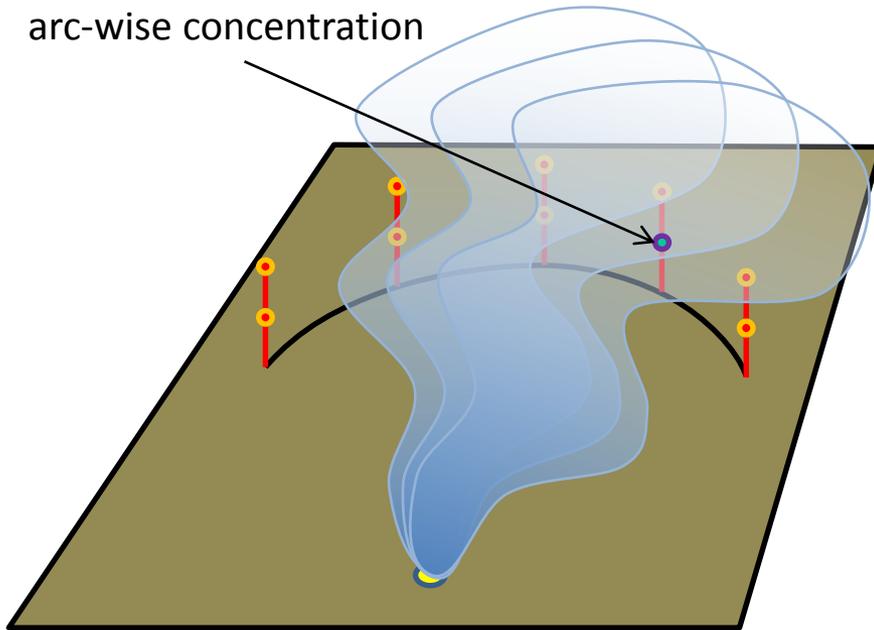


Model: Method 1

Maximum concentration at any circumferential position and at any height

Maximum Arc-Wise Concentration

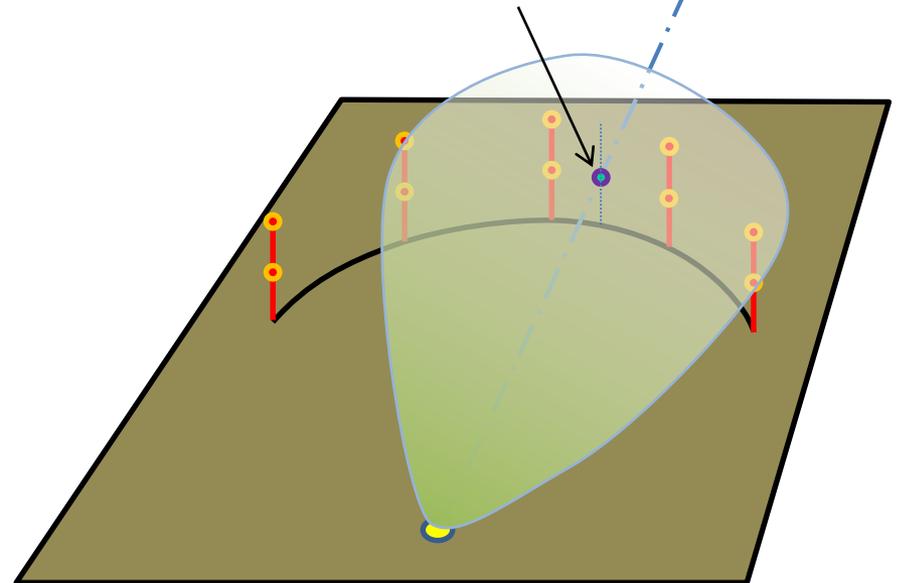
Measured maximum arc-wise concentration



Experiments

Predicted maximum arc-wise concentration

Cloud centreline

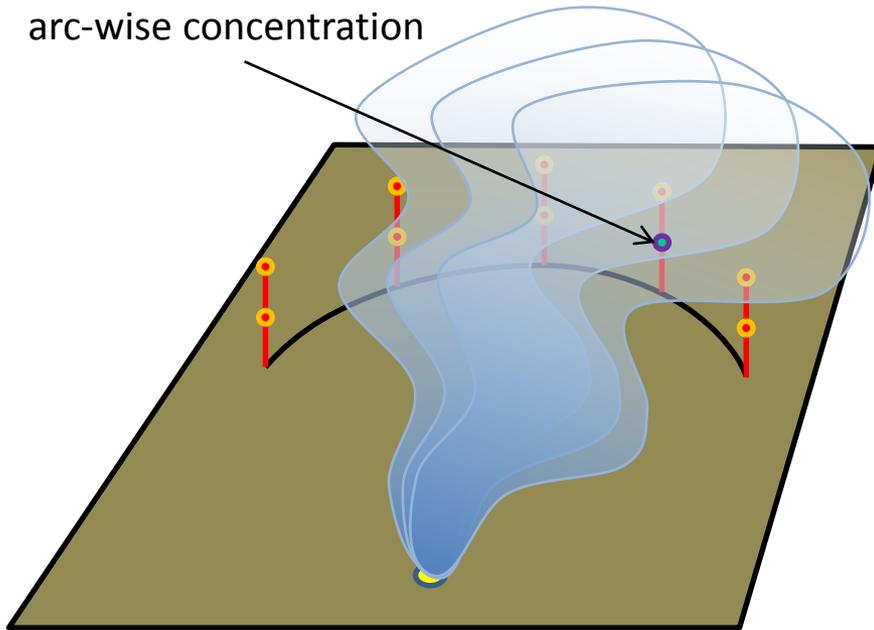


Model: Method 2

Maximum concentration at any circumferential position and at height of lowest sensors

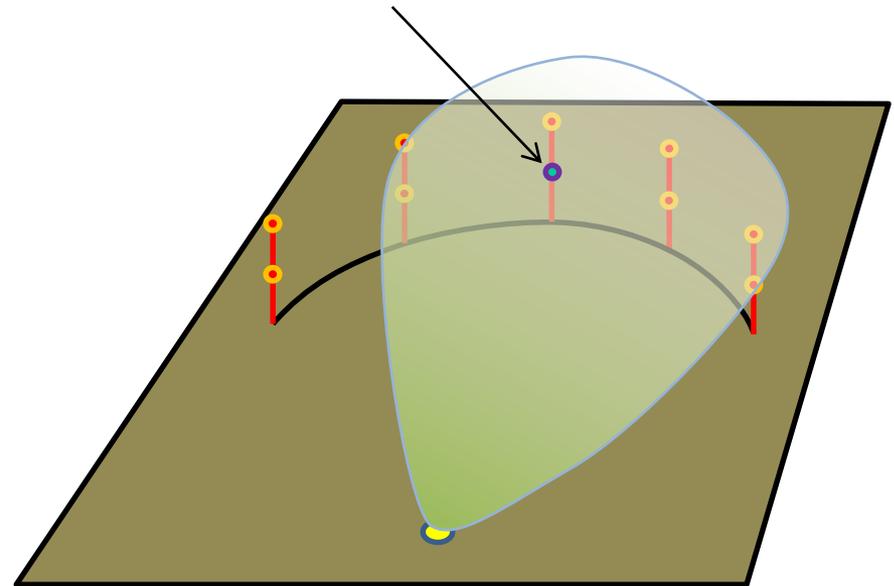
Maximum Arc-Wise Concentration

Measured maximum arc-wise concentration



Experiments

Predicted maximum arc-wise concentration



Model: Method 3

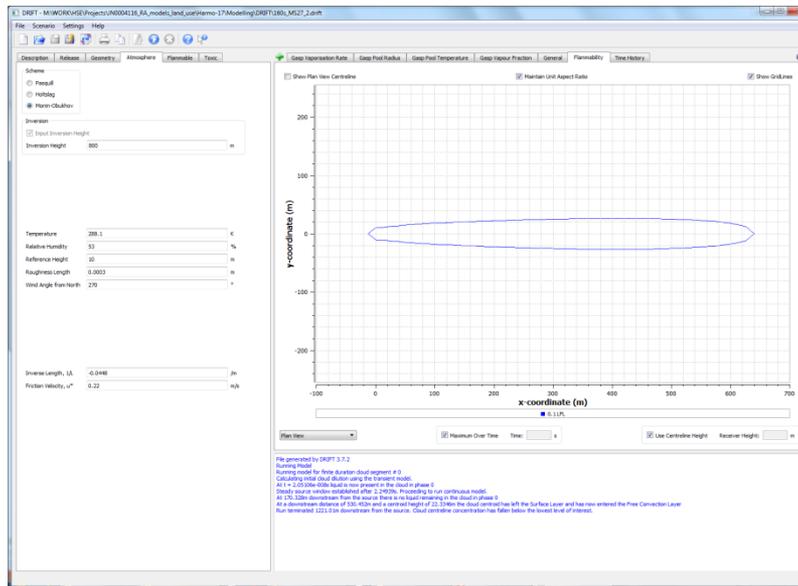
PHMSA-2010-0226 Advisory Bulletin "The maximum arc wise concentration should be based on the location of the experimental sensor data that produced the maximum arc wise concentration relative to the cloud centerline"

Maximum at any of the sensor positions



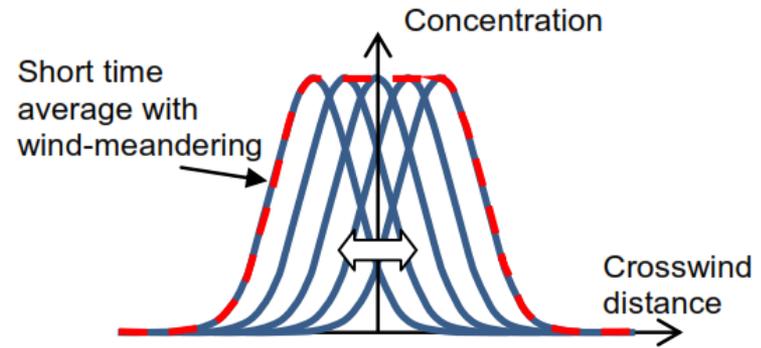
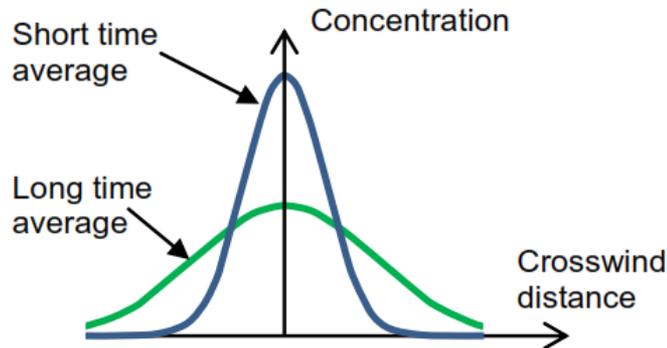
Aim & Methodology

- **Aim:** To assess how Methods 1, 2 and 3 affect the results for the field-scale experiments in the LNG MEP
 - Does it matter which method is used?
- **Methodology:** DRIFT integral dispersion model

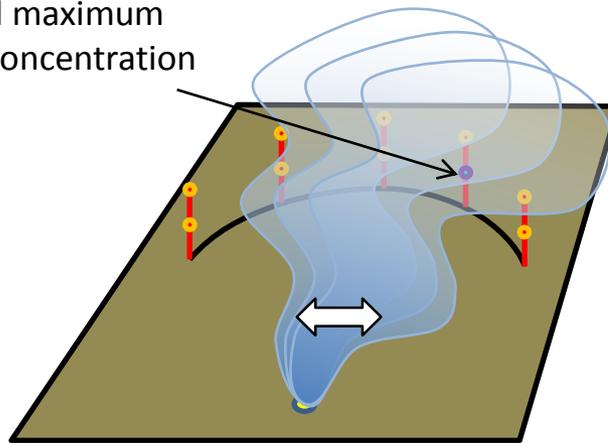


- Developed by ESR Technology
- Dense/passive/buoyant dispersion
- GASP pool evaporation model

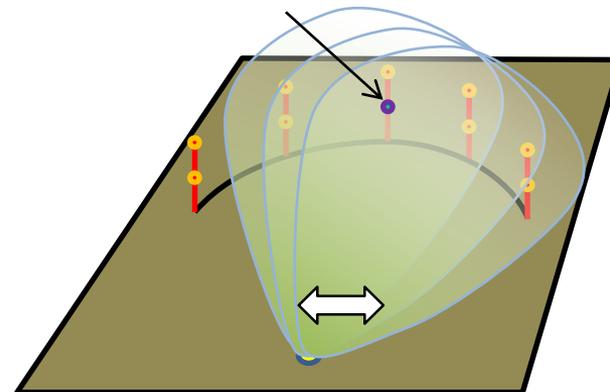
Plume Meander (Method 3a)



Measured maximum arc-wise concentration



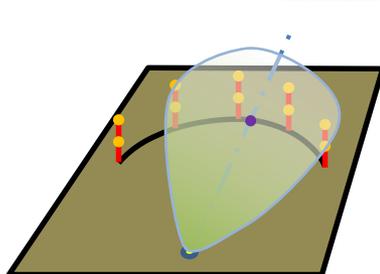
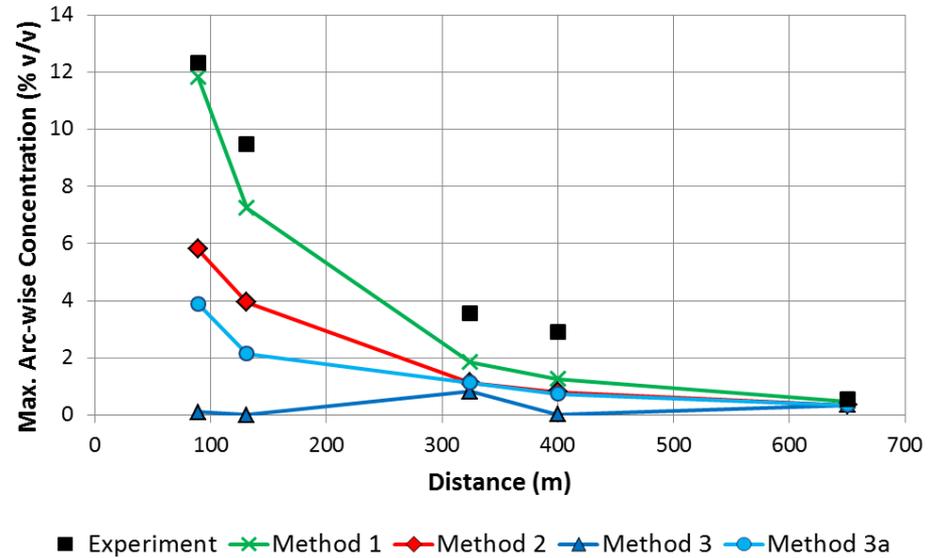
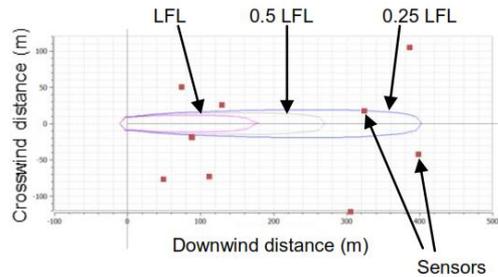
Predicted maximum arc-wise concentration



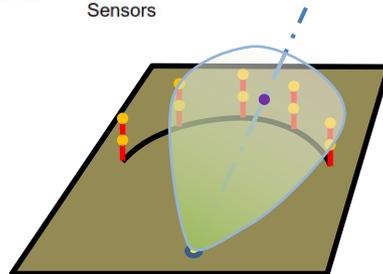
Results: Maplin Sands 27



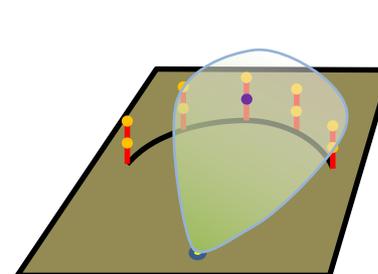
From: Colenbrander, Evans and Puttock (1984), © Shell



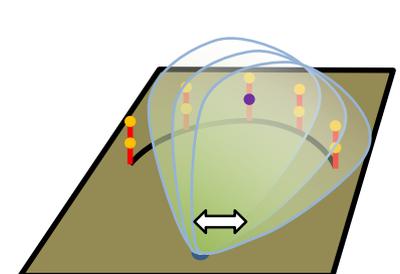
Method 1: Max. anywhere



Method 2: Max. at lowest sensor height

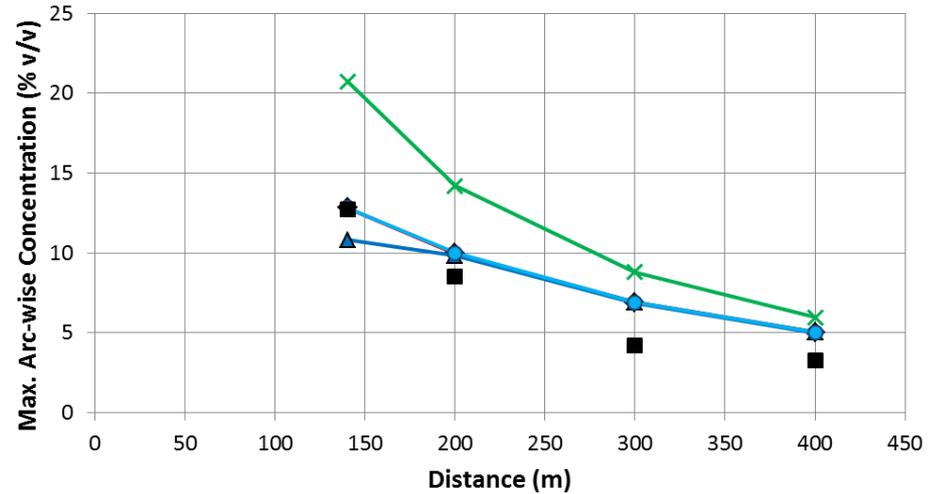
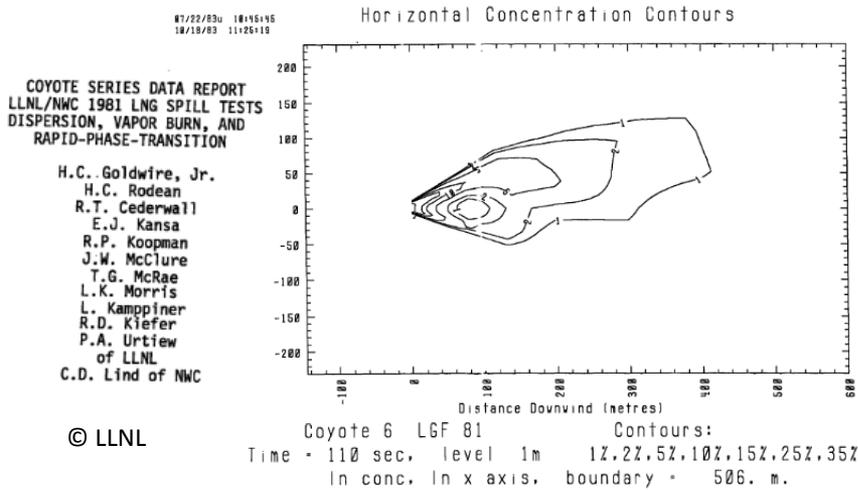


Method 3: Max. at sensor positions

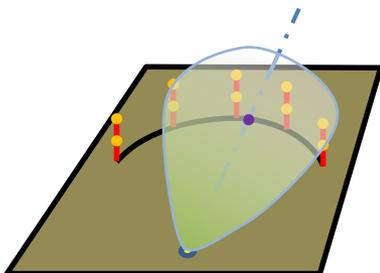


Method 3a: Wind meandering

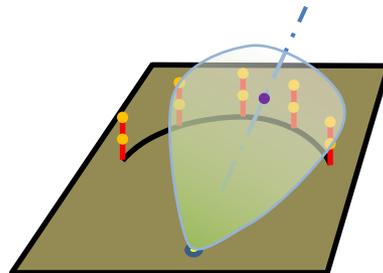
Results: Coyote 6



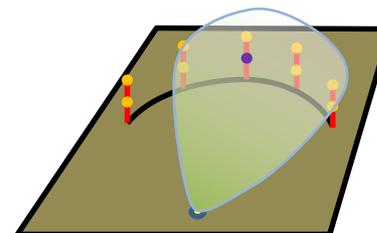
■ Experiment × Method 1 ◆ Method 2 ▲ Method 3 ● Method 3a



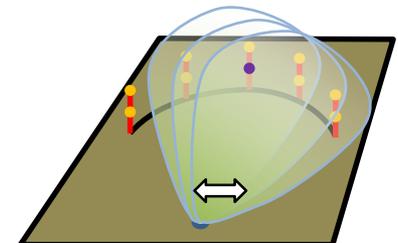
Method 1: Max. anywhere



Method 2: Max. at lowest sensor height

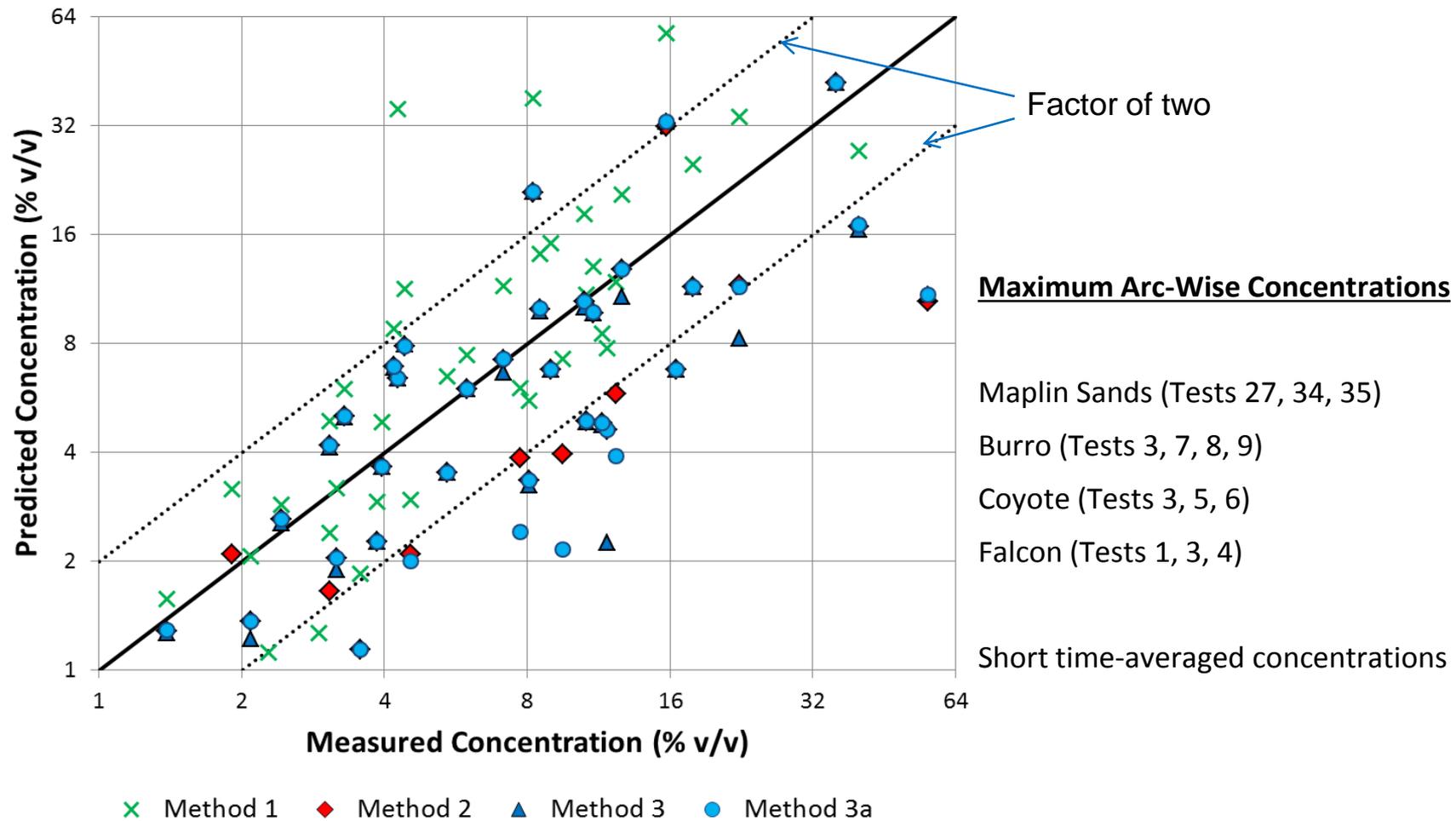


Method 3: Max. at sensor positions



Method 3a: Wind meandering

Results: Overall



Results: Overall

	Method 1	Method 2	Method 3	Method 3a
Mean Relative Bias, MRB	-0.21	0.31	0.59	0.41
Mean Relative Square Error, MRSE	0.34	0.38	1.1	0.59
Geometric Mean Bias, MG	0.79	1.4	6.6	1.9
Geometric Variance, VG	1.5	1.6	2e13	15
Factor of Two	78%	61%	54%	56%

$$MRB = \left\langle \frac{C_m - C_p}{\frac{1}{2}(C_p + C_m)} \right\rangle$$

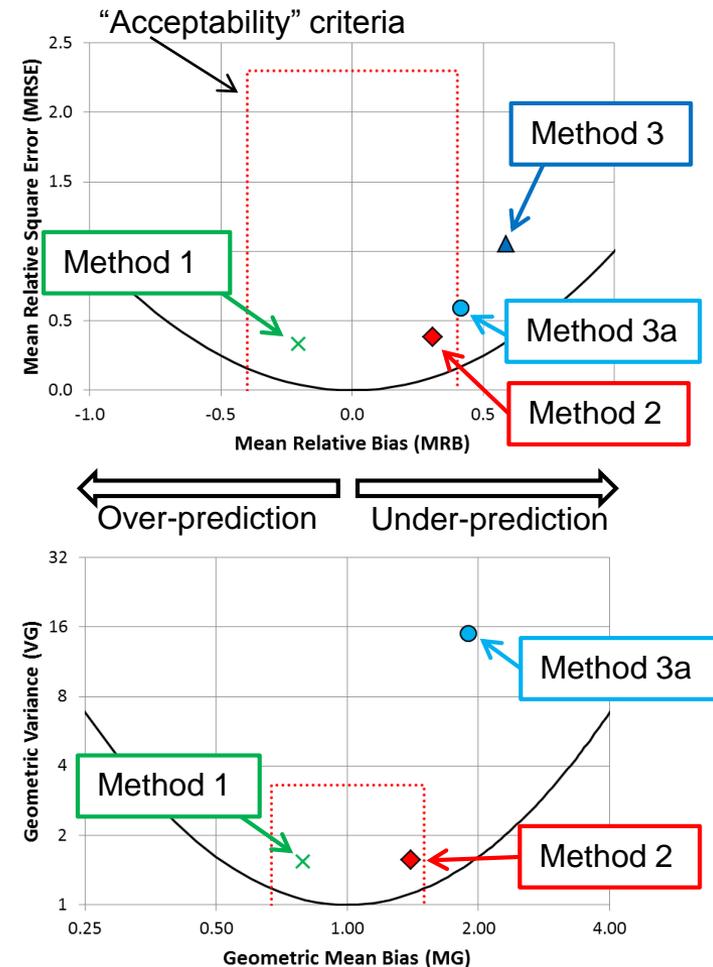
$$MRSE = \left\langle \frac{(C_p - C_m)^2}{\frac{1}{4}(C_p + C_m)^2} \right\rangle$$

$$MG = \exp \left\langle \ln \left(\frac{C_m}{C_p} \right) \right\rangle$$

$$VG = \exp \left\langle \left[\ln \left(\frac{C_m}{C_p} \right) \right]^2 \right\rangle$$

C_m = measured concentration

C_p = predicted concentration



Conclusions

- Choice of method for maximum arc-wise concentrations is important
- Depending on the choice of method, a model may be found to under/over-predict the measurements on average
- Method 3 (used by PHMSA) is more likely to indicate that a model under-predicts on average than other methods for max. arc-wise concentration
 - This is a precautionary approach given uncertainties in ensemble mean concentrations (it will tend to make the $\frac{1}{2}$ LFL exclusion zone larger)
 - It accounts for the strong vertical gradient in concentration near the ground
 - It accounts for sensors not being aligned to arcs in some experiments
 - It encourages development of plume meandering models
- Further work is needed to investigate the plume meandering model in DRIFT and the sensitivity of results to the cloud height in the near-field

Acknowledgements

We would like to thank the following for their support in producing this work:

- Julie Halliday (PHMSA)
 - Simon Rose (Oak Ridge National Laboratory)
 - Andrew Kohout (Federal Energy Regulatory Commission)
 - PHMSA
 - Shell
 - LLNL
- } For permission to use their material

This publication and the work it describes were funded by the Health and Safety Executive (HSE). Its contents, including any opinions and/or conclusions expressed, are those of the authors alone and do not necessarily reflect HSE policy.

References

- Ivings M.J., Jagger S.F., Lea C.J. and Webber D.M. (2007) Evaluating vapor dispersion models for safety analysis of LNG facilities, The Fire Protection Research Foundation, 9 May 2007.
 - <http://www.nfpa.org/research/fire-protection-research-foundation/projects-reports-and-proceedings/hazardous-materials/gases/evaluating-vapor-dispersion-models-for-safety-analysis>
- Coldrick S., Lea C.J. and Ivings M.J. (2010) Validation database for evaluating vapour dispersion models for safety analysis of LNG facilities: Guide to the LNG Model Evaluation Database, Version 11.0, 17th May 2010.
 - http://www.nfpa.org/~media/files/research/research-foundation/research-foundation-reports/hazardous-materials/lng_database_guide.pdf?la=en
- Webber D.M., Gant S.E., Ivings M.J. and Jagger S.F. (2009) LNG source term models for hazard analysis, The Fire Protection Research Foundation. Also published as Research Report RR789, Health and Safety Executive (HSE), Bootle, UK
 - <http://www.hse.gov.uk/research/rrhtm/rr789.htm>
- PHMSA Advisory Bulletin, docket PHMSA-2010-0226
 - http://phmsa.dot.gov/pv_obj_cache/pv_obj_id_B1E12F1E74C27BEAB343DEB90D621DF5BB340700/filename/ADB-10-07%20LNG%20Facilities.pdf
- FERC evaluation of DEGADIS 2.1
 - <https://www.ferc.gov/industries/gas/indus-act/lng/degadis-report.pdf>
- PHMSA evaluation of PHAST v6.6 and v6.7
 - <http://www.regulations.gov/#!docketDetail;D=PHMSA-2011-0075>
- PHMSA evaluation of FLACS 9.1r2
 - <https://www.regulations.gov/#!docketDetail;D=PHMSA-2011-0101>