

# Smoke plume from fire lagrangian simulation: dependence on drag coefficient and resolution

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## Introduction

A numerical simulation of the plume dispersed from a fire is performed using the Lagrangian stochastic particle model SPRAYWEB and the results are compared to a field experiment, carried out in August 2013 in Idaho (USA). Here we want to assess the dependence of the plume rise scheme on the values chosen for the drag coefficient and the cell size.

## The plume rise scheme

The plume rise scheme (Alessandrini et al., 2013) is based on the Lagrangian description of the plume evolution in terms of particle trajectories, while the temperature and momentum differences, which are responsible for the plume buoyancy, are calculated on a fixed grid. At each time step  $\Delta t = t_1 - t_0$  temperature and momentum differences ( $\Delta T$  and  $w_c$  respectively) between each grid cubic cell and the surrounding environment are computed using the following equations

$$\Delta T(t_1) = \Delta T(t_0) + \Gamma(z_c)w_c(t_0)\Delta t + 0.0098w_c(t_0)\Delta t$$

$$w_c(t_1) = w_c(t_0) + \frac{\Delta T_c(t_1)}{\Delta T_c + T_a(z_c)}g\Delta t - \frac{0.5C_D S w_c^2(t_0)\rho_a}{\rho_p V_c}\Delta t$$

where  $z_c$  is the cell height,  $T_a$  the ambient temperature,  $g$  the gravity,  $C_D$  the drag coefficient,  $S$  and  $V_c$  the cell section and volume,  $\rho_a$  and  $\rho_p$  the ambient and plume density. This plume rise scheme is not based on an analytical model and the only two assumptions required are the drag coefficient value and the cell size.

## Drag coefficient models

There is not a generally accepted value in the literature for the drag coefficient. Four drag coefficient expressions which depend on the Reynolds number of the cells ( $Re_c = \phi \frac{|U_c|}{\nu}$ , where  $\phi$  is the equivalent cell diameter,  $U_c$  is the cell vertical velocity and  $\nu$  is the kinematic viscosity of air), are tested.

Table: Drag coefficient expressions

Author	$C_D$ expression
Turton and Levenspiel (1986)	$C_D = \frac{24}{Re_c}(1 + 0.173Re_c^{0.657}) + \frac{0.413}{1+16300Re_c^{-1.09}}$ , if $Re_c < 2 * 10^5$
Brown and Lawler (2003)	$C_D = \frac{24}{Re_c}(1 + 0.15Re_c^{0.681}) + \frac{0.407}{1+8710Re_c^{-1}}$ , if $Re_c < 2 * 10^5$
Cheng (2009)	$C_D = \frac{24}{Re_c}(1 + 0.27Re_c)^{0.43} + 0.47(1 - \exp(-0.04Re_c^{0.38}))$
Mikhailov and Silva Freire (2013)	$C_D = \frac{777((\frac{669806}{875})+(\frac{114976}{1155})Re_c+(\frac{707}{1380})Re_c^2)}{646Re_c((\frac{32869}{952})+(\frac{924}{643})Re_c+(\frac{1}{385718})Re_c^2)}$

The first three expressions presented in the table above are similar, as a sort of Stokes' law extended for higher Reynolds numbers, but with different constants derived by fitting experimental data. The latter is derived from the Shanks transformation of Goldstein series (Goldstein, 1929, Shanks, 1955) improved by fitting its coefficients directly to experimental data.

## Taylor diagram

The two most faithful models are those of Cheng (2009) and Brown and Lawler (2003) since their points are closest to that of the observations.

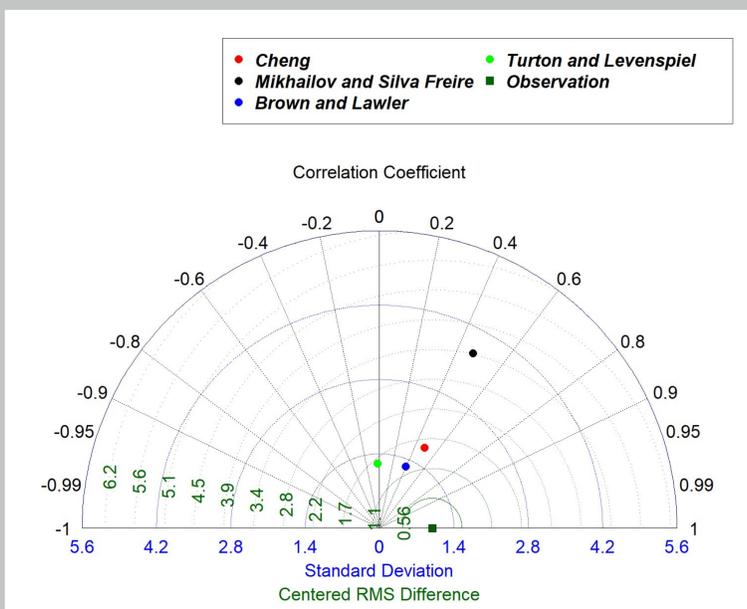


Figure: Taylor diagram for the four drag coefficient expressions

## Maximum height

We estimated maximum plume height considering two vertical standard deviation of the plume distribution above the mean particles height.

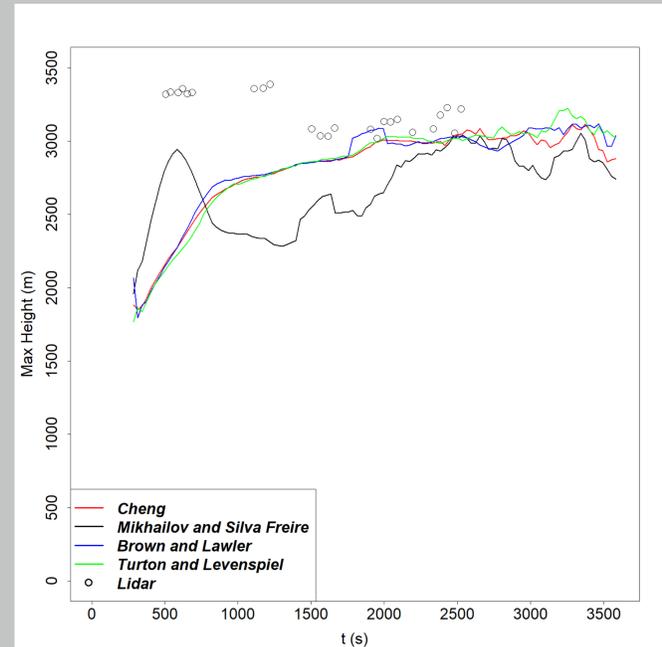


Figure: Maximum plume height trend

## QQ-plots

QQ-plot of the models deriving from the Stokes law is shown on the left; the one of the model from the Shanks transformation of Goldstein series is shown on the right.

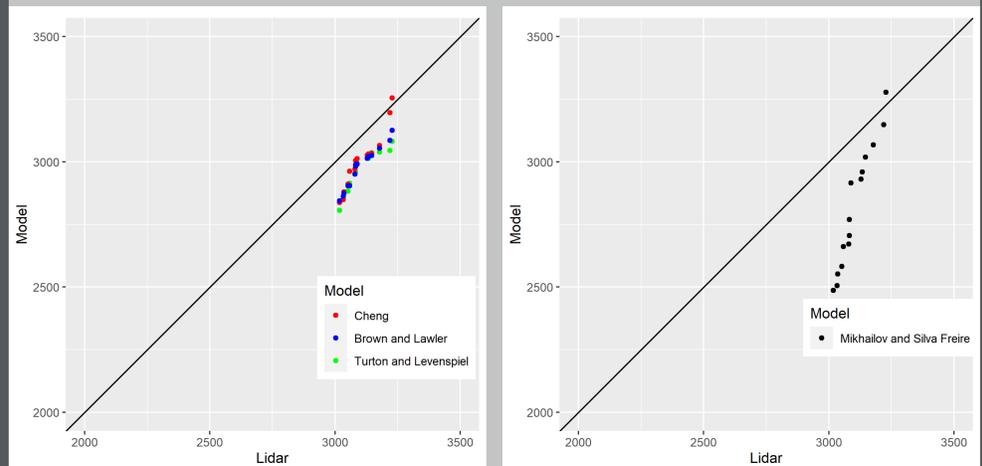


Figure: Models qq-plots

## Conclusions

For this type of application the models deriving from the Stokes law have a better performance. In particular, the models of Cheng (2009) and Brown and Lawler (2003) give results that better agree with the observations. The model of Brown and Lawler (2003) can only be applied in case of Reynolds numbers less than  $2 \times 10^5$ , while the one of Cheng (2009) has no restrictions and this makes it the best choice for our purposes. We are now working on other case studies to consolidate these results. Regarding the horizontal resolution we did not find a strong dependence of the results in case of small prescribed fires

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## References

- Brown, P. P., and Lawler, D. F., 2003: Sphere drag and settling velocity revisited. *Journal of environmental engineering*, 129(3), 222-231.
- Cheng, N. S., 2009: Comparison of formulas for drag coefficient and settling velocity of spherical particles. *Powder Technology*, 189(3), 395-398.
- Ferrero, E., Alessandrini, S., Anderson, B., Tomasi, E., Jimenez, P., and Meech, S., 2019: Lagrangian simulation of smoke plume from fire and validation using ground-based lidar and aircraft measurements. *Atmospheric Environment*, 213, 659-674.
- Mikhailov, M. D. and Freire, A. S., 2013: The drag coefficient of a sphere: An approximation using Shanks transform. *Powder technology*, 237, 432-435.
- Turton, R. and Levenspiel, O., 1986: A short note on the drag correlation for spheres. *Powder technology*, 47(1), 83-86.